Lecture 21 - Nonlinear Equations II

- Prayer/Spiritual Thought
- Announcements

Outline

- 1. Solve blocks with parameters
- 2. Best practices with solve blocks
- 3. Debugging solve blocks

1. Solve blocks with parameters

- A. Explanation
- Sometimes you want to solve a nonlinear equation multiple times while varying a parameter.
- We can do this by making a solve block where:
 - 1. We leave the parameter *unspecified*
 - 2. We define a function using **find**
- This is best explained with an example:
- B. Example

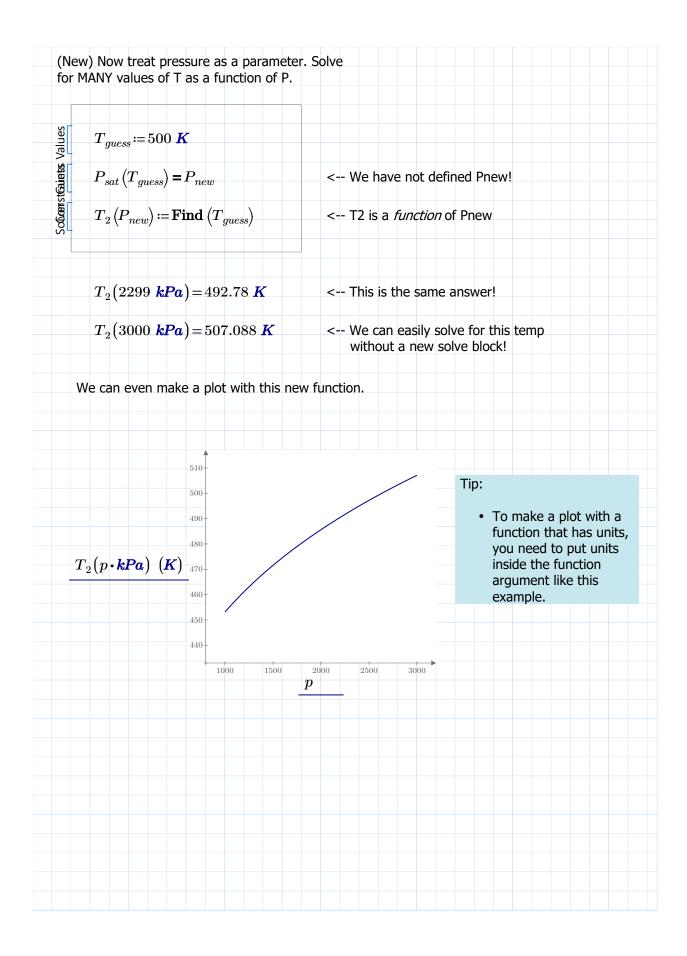
Suppose we are trying to find the temperature of a saturated vapor using a vapor pressure correlation:

$$P_{sat}(T) \coloneqq \exp\left(73.649 - 7258.2 \cdot \left(\frac{T}{K}\right)^{-1} - 7.3037 \cdot \ln\left(\frac{T}{K}\right) + 4.1653 \cdot 10^{-6} \cdot \left(\frac{T}{K}\right)^{2}\right) \cdot Pa$$

(Old) Typical Solve block

| P≔2299 • kPa | This is a single pressure where we |
|---------------------|------------------------------------|
| | want to find the temperature. |

$$\begin{aligned} & T_{guess} \coloneqq 500 \ \textbf{K} \\ & \text{Set} \\ & P_{sat} \left(T_{guess} \right) = P \\ & \text{T}_1 \coloneqq \text{Find} \left(T_{guess} \right) = 492.78 \ \textbf{K} \end{aligned}$$



| | practices with solve blocks |
|------------------------|---|
| A. Expl | anation |
| powe unde • This | solver in Excel, solve blocks in Mathcad are quite powerful. However, solve blocks are not a erful, and they can fail to give an answer. There is a lot of algorithmic complexity happening erneath the hood. means there are some best practices (rules you should generally follow unless you have a on not to) that help you get an answer when using solve blocks. |
| B. List | of best practices |
| | herever possible, reduce the number of equations and variables. range equations to avoid |
| | fractional powers (e.g. square roots) logs poles (infinite discontinuities) |
| 2 М | ake a smart guess. Your guess should: |
| | Obey the constraints of the problem Make physical sense Be the right sign Be guided by a plot |
| C. Exar | s to be close enough to converge to an answer. mples |
| | |
| | mples Reducing equations Remember our vapor/liquid equilibrium problem from last time: $y_1 \cdot P = x_1 \cdot P_{sat_1}$ $y_2 \cdot P = x_2 \cdot P_{sat_2}$ $y_1 + y_2 = 1$ $x_1 + x_2 = 1$ |
| | mples Reducing equations $y_1 \cdot P = x_1 \cdot P_{sat_1}$ $y_2 \cdot P = x_2 \cdot P_{sat_2}$ |
| | mples Reducing equations Remember our vapor/liquid equilibrium problem from last time: $y_1 \cdot P = x_1 \cdot P_{sat_1}$ $y_2 \cdot P = x_2 \cdot P_{sat_2}$ $y_1 + y_2 = 1$ $x_1 + x_2 = 1$ $ln\left(P_{sat_i}\right) = A_i - \frac{B_i}{T + C_i}$ |
| | mples Reducing equations Remember our vapor/liquid equilibrium problem from last time: $y_1 \cdot P = x_1 \cdot P_{sat_1}$ $y_2 \cdot P = x_2 \cdot P_{sat_2}$ $y_1 + y_2 = 1$ $x_1 + x_2 = 1$ $ln\left(P_{sat_i}\right) = A_i - \frac{B_i}{T + C_i}$ Given quantities |

$$\begin{array}{c} \text{(Bad example)} - \text{Using too many unnecessary equations} \\ \hline \\ \textbf{x}_1 \coloneqq 0.4 \quad \textbf{x}_2 \coloneqq 0.5 \quad \textbf{y}_2 \coloneqq 0.1 \\ T \coloneqq 50 \quad P_{\text{sot},1} \coloneqq 100 \quad P_{\text{sut},2} \simeq 100 \\ T \coloneqq 50 \quad P_{\text{sot},1} \coloneqq 100 \quad P_{\text{sut},2} \simeq 100 \\ \textbf{y}_1 \cdot P = \textbf{x}_1 \cdot P_{\text{sut},1} \quad \textbf{x}_1 + \textbf{x}_2 = 1 \\ \textbf{y}_2 \cdot P = \textbf{x}_2 \cdot P_{\text{sut},2} \quad \textbf{y}_1 + \textbf{y}_2 = 1 \\ \textbf{y}_2 \cdot P = \textbf{x}_2 \cdot P_{\text{sut},2} \quad \textbf{y}_1 + \textbf{y}_2 = 1 \\ \textbf{in} \left(P_{\text{sot},1} \right) = A_1 - \frac{B_1}{T + C_1} \\ \textbf{in} \left(P_{\text{sot},2} \right) = A_2 - \frac{B_2}{T + C_2} \\ \textbf{Find} \left(\textbf{x}_1, \textbf{x}_2, \textbf{y}_2, P_{\text{sot},1}, P_{\text{sot},2}, \textbf{T} \right) = \begin{bmatrix} 0.173 \\ 0.827 \\ 0.67 \\ 229.396 \\ 97.175 \\ 109.131 \end{bmatrix} \\ \begin{array}{c} \text{Luckily this one still converges to the right answer.} \\ \textbf{(Good example)} - \text{Eliminate unnecessary intermediates} \\ \textbf{(Good example)} - \text{Eliminate unnecessary intermediates} \\ \textbf{y}_1 \cdot P = \textbf{x}_1 \cdot exp \left(A_1 - \frac{B_1}{T + C_1} \right) \\ \textbf{(} 1 - \textbf{y}_1 \right) \cdot P = (1 - x_1) \cdot exp \left(A_2 - \frac{B_2}{T + C_2} \right) \\ \textbf{W}_1 = \textbf{Find} \left(x_1, T \right) = \begin{bmatrix} 0.173 \\ 109.131 \end{bmatrix} \\ \textbf{M}_2 = \textbf{M}_2 = 0.5 \\ \textbf{M}_3 = 0.5 \\ \textbf{M}_4 = 0.5 \\ \textbf{M}_4$$

| (ii) Bad | guesses | |
|--|---|---|
| | Consider the liquid-liquid equilibrium between a po and a solvent | olymer |
| | $\mu_1\left(\phi_a\right) = \mu_1\left(\phi_b\right)$ | |
| | $\mu_2\left(\phi_a\right) = \mu_2\left(\phi_b\right)$ | |
| | $\mu_{1} = ln(\phi) + (1 - \phi) \cdot \left(1 - \frac{1}{N}\right) + \chi \cdot (1 - \phi)^{2}$ | |
| | $\mu_{2} = \frac{1}{N} \ln(1-\phi) + \phi \cdot \left(\frac{1}{N} - 1\right) + \chi \cdot \phi^{2}$ | |
| | where phi_a, phi_b are the volume fractions of the solvent in phase a and b respectively. N and Chi a parameters which describe the polymer size and interaction between polymer and solvent. Assume $N = 10$ and $\chi = 2.5$. | ire |
| | $N \coloneqq 10$ $\chi \coloneqq 2.5$ | |
| | $\mu_{1}(\phi) \coloneqq \ln(\phi) + (1-\phi) \cdot \left(1 - \frac{1}{N}\right) + \chi \cdot (1-\phi)^{2}$ $\mu_{2}(\phi) \coloneqq \frac{1}{N} \ln(1-\phi) + \phi \cdot \left(\frac{1}{N} - 1\right) + \chi \cdot \phi^{2}$ | The logs are unavoidable here. This makes this problem hard. |
| | $N = \left(\begin{array}{c} 1 \\ 1 \end{array} \right) \left(\begin{array}{c} 1 \end{array} \right) \left(\begin{array}{c} 1 \\ 1 \end{array} \right) \left(\begin{array}{c} 1 \end{array} \right) \left(\begin{array}{c} 1 \\ 1 \end{array} \right) \left(\begin{array}{c} 1 $ | |
| and the second states of the s | $\phi_{a} := 0.1 \qquad \phi_{b} := 0.999$ $\mu_{1}(\phi_{a}) = \mu_{1}(\phi_{b}) \qquad \mu_{2}(\phi_{a}) = \mu_{2}(\phi_{b})$ | < Try different guesses: * negative * out of physcial bounds (0, 1) * A guess where phi_a is close |
| Solvañon etrainfa ao | $\sum_{a=1}^{n} \sum_{i=1}^{n} \sum_{j=1}^{n} \sum_{i=1}^{n} \sum_{i$ | to 0 and phi_b is very close to 1 will work. |
| | Find $(\phi_a, \phi_b) = \begin{bmatrix} 0.04275238\\ 0.99999992 \end{bmatrix}$ | < These should be different numbers. If they are the same, it is not the right answer. |
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| 3. Debugging solve blocks |
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| A. Explanation |
| It can be hard to find syntax errors or other mistakes inside solve blocks. Like programming, good debugging skills are won with practice and experience, but some general tips can also help. |
| B. List of debugging techniques |
| Check to make sure that all functions defined before the solve block work properly Copy the LHS and RHS of the equations in the solve block to check: |
| Calculation Units |
| Order of magnitude |
| Don't over/under specify the problem. In other words the number of guesses should equal the number of equations which should also equal the number of variables in the find statement. Ensure that each solve block has: |
| Guesses Equations Find |
| Double check your variables. Make sure the guesses, equations, and find are all written with the same variables. |
| C. Examples |
| Debug the following solve block |
| $\rho := 55.19 \frac{kg}{m^3} \qquad \mu := 0.00087645 \cdot Pa \cdot s \qquad \varepsilon := 1.524 \cdot 10^{-3} \cdot mm$ |
| $D \coloneqq 1.91 \cdot cm \qquad \Delta P \coloneqq -70 \cdot kPa \qquad Len \coloneqq 20 \cdot m$ |
| $ \underbrace{ \begin{array}{c} \underset{g \in \mathcal{G}}{\overset{g}{\underset{g \in \mathcal{G}}{\underset{g \in \mathcal{G}}{$ |
| $\frac{\Delta P}{\rho} = -f_g \cdot \frac{Len}{D} \cdot \frac{v_g^2}{2} \qquad \frac{1}{\sqrt{f_g}} = -2 \cdot \log\left(\frac{\varepsilon \cdot D}{3.7} + \frac{2.51}{\frac{\rho \cdot D \cdot v_g}{\mu} \cdot \sqrt{f_g}}\right)$ |
| $ \underbrace{\overset{\mathtt{v}}{\overset{t}}{\overset{t}}{\overset{t}}{\overset{t}}{\overset{t}}{\overset{t}}}}}} = ? $ |
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